



STEAG Energy Services Approach to Higher Flexibilization “Tools and Results”

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- **Decreased, but still robust low load operation**
- **Faster start-up and ramping dynamics**
- **Controllability: proof of potential to provide grid services (e.g. frequency control)**

- **Increased wear and tear of equipment**
- **Revenue loss due to reduced full load operation**
- **Diligent adjustment of O&M procedures**
- **Need to enhance overall plant performance and efficiency**

The Triad that Makes Us Unique

GERMAN
ENGINEERING

100,000 MW
across all
technologies

O&M
PRACTICES

Currently 6,500 MW
full-scope O&M for
third parties ...

... and O&M manage-
ment support for
further 3,500 MW.

IT-BASED
PROCESS
OPTIMIZATION

>700
IT systems
delivered

Main topics of flexibilization

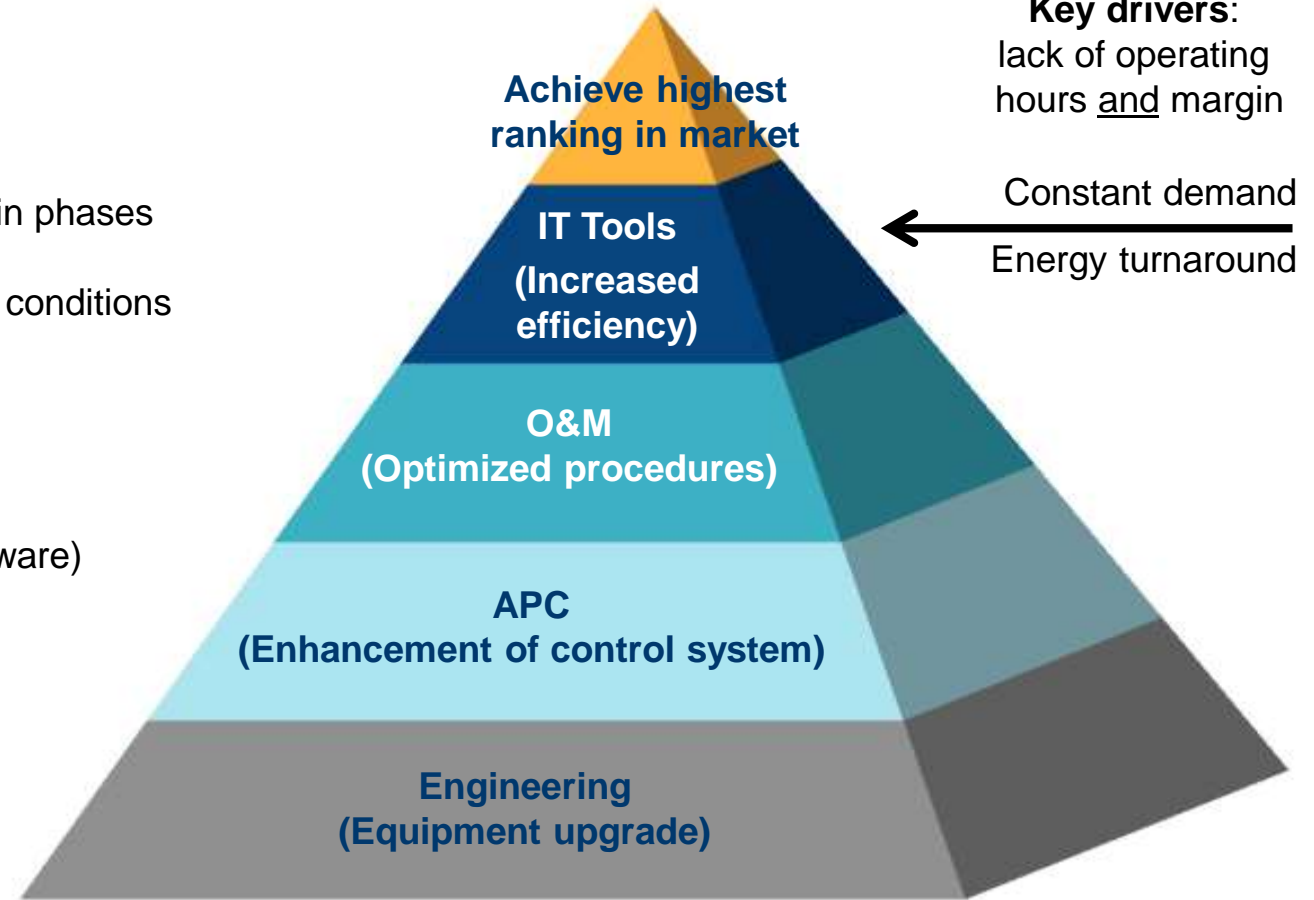
- › Start-up optimization: reproducible, faster, cheaper due to saving start-up fuel
- › Minimum load reduction: keep plant in operation at negative margin phases to avoid start-up costs
- › Increased ramp rates to ensure a fast reaction to changed market conditions

Measures of flexibilization

- › Identification of limiting components
- › Control optimization (software modification)
- › Evaluation and optimization of components and aggregates (hardware)

Improvement of O&M processes

- › Evaluation of best-practice procedure, e.g. for start-up, shut-down, overhauls etc.
- › Harmonization of organizations and processes within the fleet
- › Workshops



- **Retrofitting with regards to mechanical engineering as well as process engineering**
- **Enhancement of the underlying control loops**
- **Improved utilization of system inherent storage capabilities**
- **Applying advanced process control (APC) based on physical modelling as well as neural network solutions**
- **Optimization of Ramp rate, SH/RH spray control & Combustion Process etc.**
- **Implementation of online lifetime monitoring**
- **Upgrading and adjustment of respective operational procedures**
- **Awareness building and know-how transfer sensitizing the operators**
- **Applying simulator or on the job training**

Optimization of relevant subordinate controls:

› Analysis of subordinate controls like:

- Life steam temperature control, fuel control, feed water control
- Individual analysis, adaption and optimization of each subordinate control
- Recommendation for exchange of sensors, actuators and electronic I&C cards if necessary

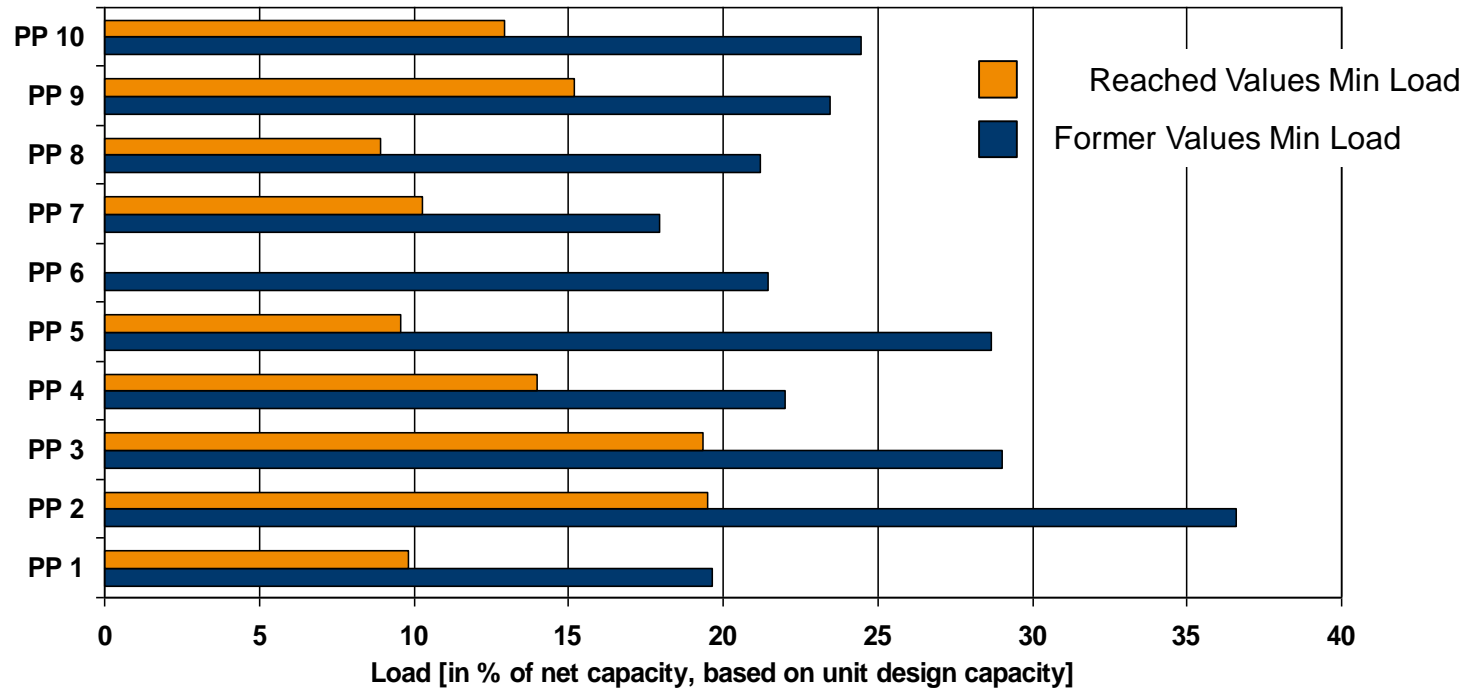
› Simple modifications:

- Control concepts are based on standards
- Control is kept as simple as possible
- The Advanced model-based control unit works as a simulation environment
- Modifications first implemented by customer after successful testing

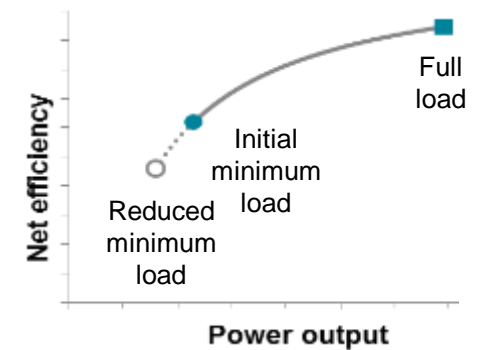
› Reduction of boiler minimum load:

- Obtained by optimization of subordinate controls and effective testing

Big potential beyond the initial design



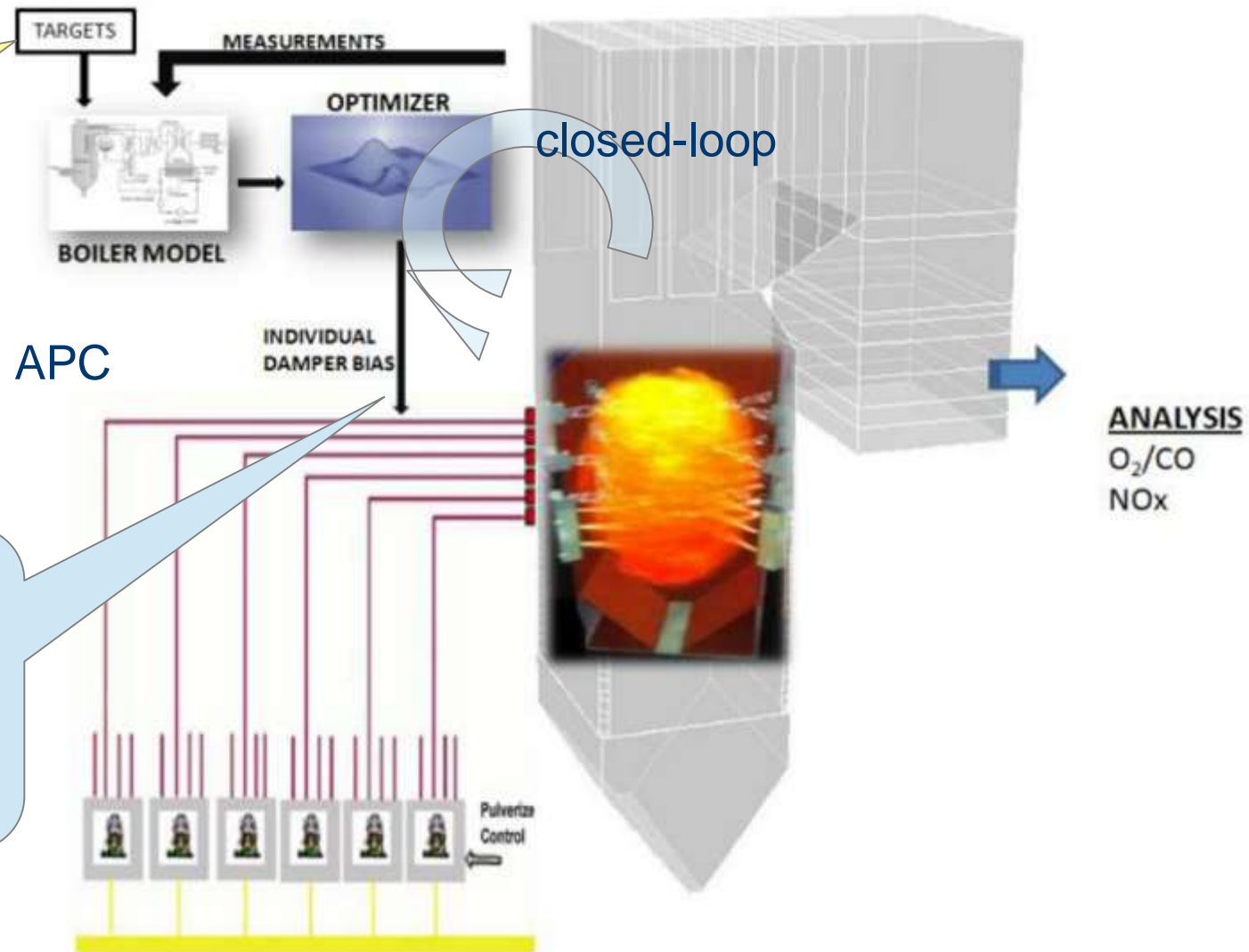
Reference plants in Germany were built between 1970 – 1990



PiT Navigator - APC Solution for Optimization

Targets to be optimized:
Temperature imbalances
Metal temperatures
Steam temperatures
Efficiency
NOx

Outputs (Biases) to be controlled:
Auxiliary air dampers
Cornerwise burner tilts
Over fire air dampers
Mill loading
RH/SH-spray flows

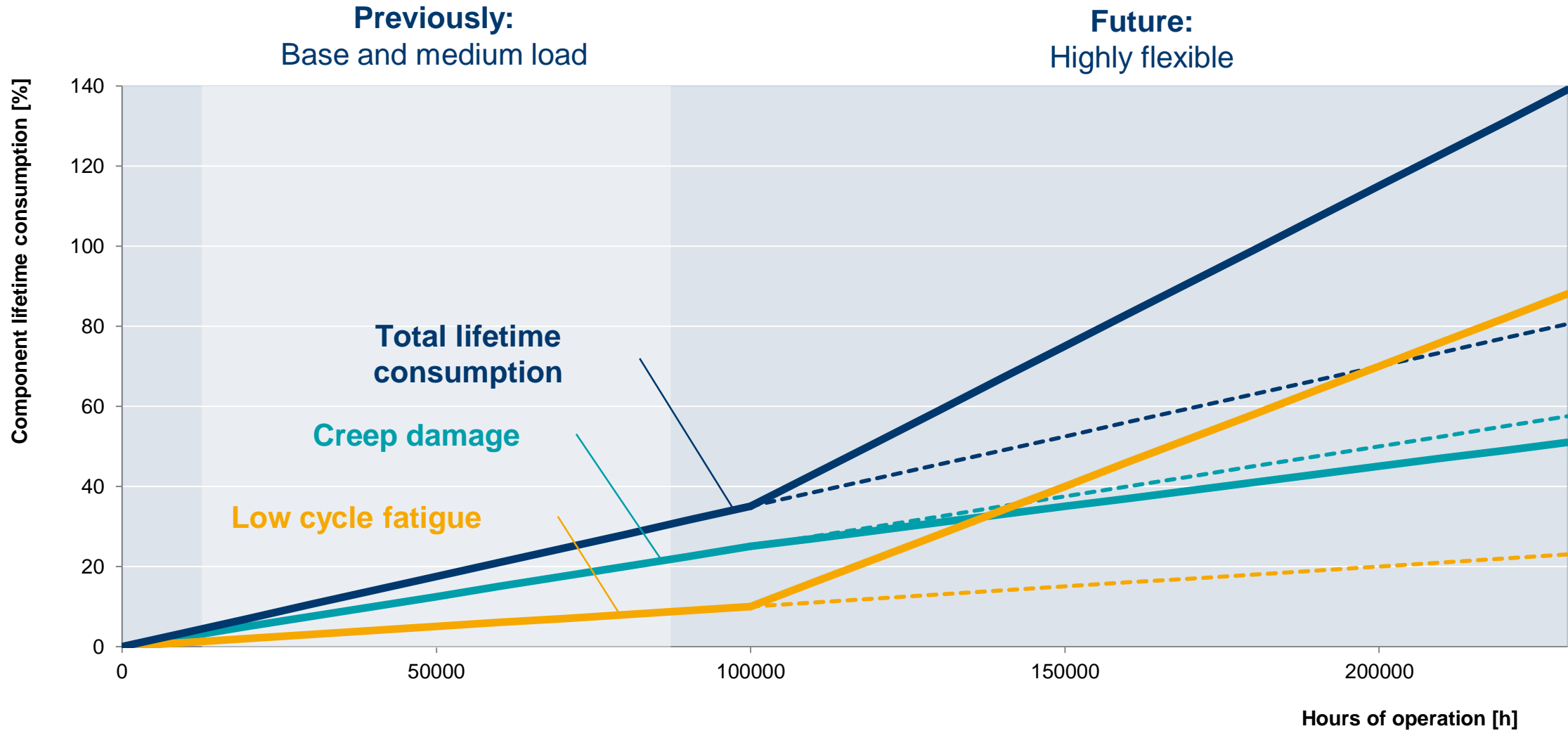


Achieved Improvements	From normal operation	To Pit Navigator	Improvement
Av. duration of RH-Metal Temperature excursion	13min/d	5.9min/d	>50%
Av. RH-Steam Temperature	532.2°C	535.2°C	3K
Av. RH-Spray	49.8t/h	43.9t/h	6t/h
Av. SH-Steam Temperature	538.4°C	539.2°C	0.8K

Unit heat rate improvement of 5 kcal/kWh by higher average steam temperatures and reduced RH-spray

- **Calculation of fatigue by online life time monitoring system**
- **Clasification of starts / Stress collectives**
- **How to meet the requirement to double the number of start-ups**

Increased Stress Due to Load Changes



Calculatory Component Life Time Consumption

Extrapolation of the Life Time Consumption

Year	Operating Hours [h]	D _F [%]	D _{F.RES} [%]	D _C [%]	D _{TOTAL} [%]
2014	7735	1,88	1,02	1,89	3,77

Table 1: Lifetime consumption for a selected component

Operating Hours [h]	D _f [%]	D _c [%]	D _{total} [%]
200.000h	48,6	48,9	97,5

Table 2: Linear extrapolation of the component lifetime consumption for 200,000 h

At first, apparently no potential for doubling the number of start-ups

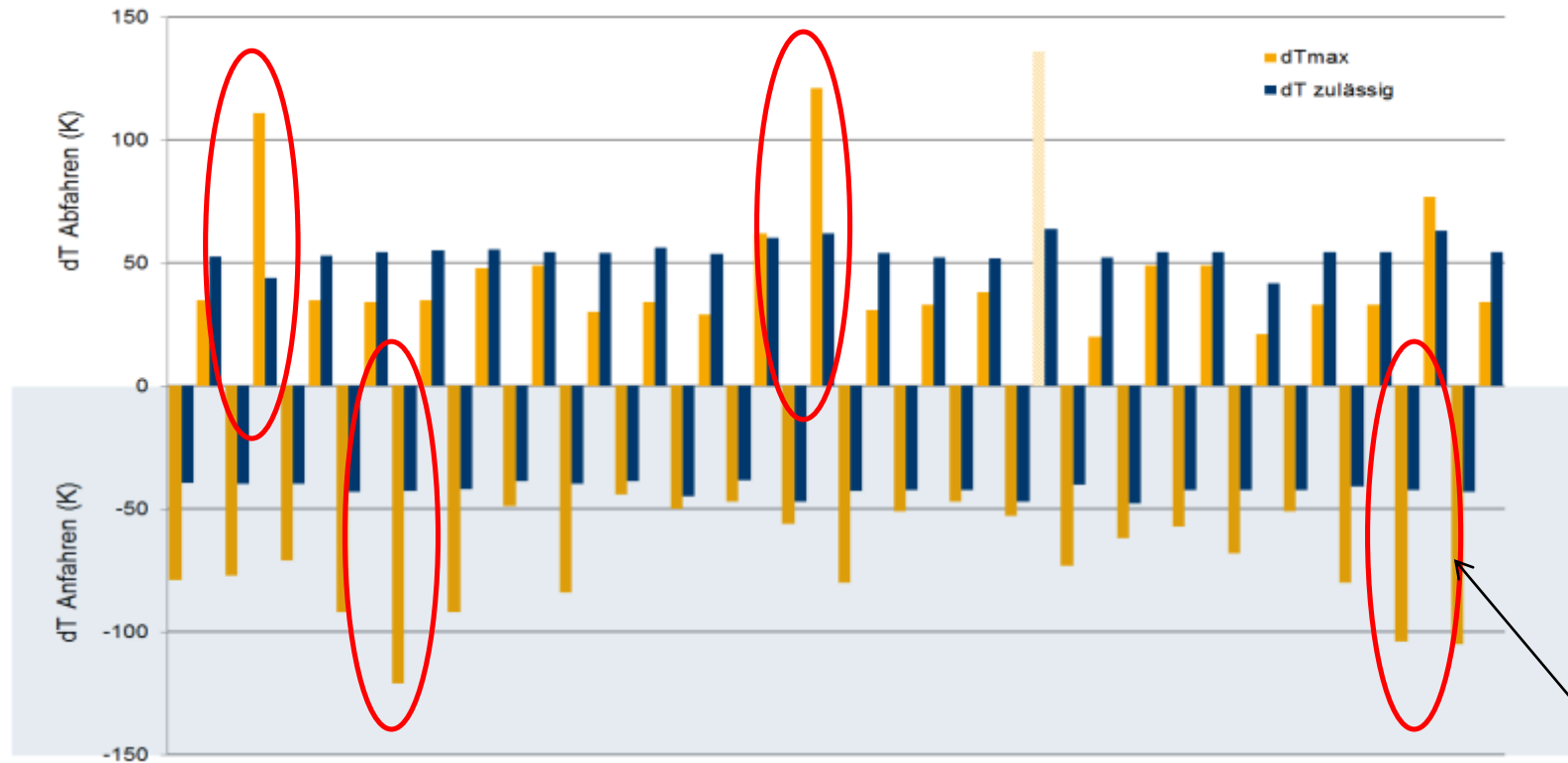
Start Type	Minimum Cycle Pressure	Minimum Cycle Temperature	Down Time
Cold Start	0 bar	>20 °C	>48h
Warm Start	0 bar	>80 °C	<48h
Hot Start	0 bar	>250 °C	<8h

Table 1: Criteria for the classification of cold, warm, and hot starts (downtime most important)

Start Type	Number	dT_{max} [K]	$dT_{max,mean}$ [K]	Σ_{max} [N/mm ²]	$\Sigma_{max,mean}$ [N/mm ²]
Cold Start	4	-84	-76	-502	-432
Warm Start	17	-121	-69	-709	-389
Hot Start	3	-77	-70	-436	-396
Shut Down	24	111	49	804	347

Table 2: Actual stress collective of a thick-walled component

Identification of critical events



high temperature difference =>
high thermal stress =>
high fatigue

Exceedance of the admissible temperature difference during start-up, shortfall during shutdown

Potential for adjusting the admissible limits exists.

Lifetime Consumption per Warm Start at Optimized Mode of Operation

Event	Df [%]	Number per Year	Df per Year [%]
WS_{,max} + Shut Down_{,max}	0,58	2	1,16

Table 3: Lifetime consumption due to critical cycle (warm start + shutdown)

Reduction of the lifetime consumption per year by 1.16% conceivable.

Operating Hours [h]	Df [%]	D _{total} [%]	D _{f,optimiert} [%]	D _{total,optimiert} [%]
200.000h	48,6	97,5	18,6	67,5

Table 4: Linear extrapolation to 200,000h of the stress determined in 2014 (with and without consideration of an optimized mode of operation)

By avoiding critical conditions, reserves for doubling the number of start-ups can be generated.

- **Adaption to flexible operation requires detailed knowledge of fatigue**
- **Online monitoring of fatigue provides this knowledge to plant engineers**
- **Avoidance of very fast ramping enables for increasing the number of starts**

Overview of Selected References

Project	Power Plant Walsum Unit 10/9
Country	Germany
Client	STEAG GmbH
Technical Data	800 MW / 410 MW – Once through boiler
Scope of Services	Minimum load reduction / Frequency control / start-up optimization – Studies as well as implementation
Project Finalization / Duration	Since 2010 – ongoing

Project	Power Plant Bexbach
Country	Germany
Client	STEAG GmbH
Technical Data	780 MW – Once through boiler
Scope of Services	Frequency control – Studies as well as implementation
Project Finalization / Duration	2015 – 2017

Project	PPs Guacolda / Bocamina Unit 1/2 / Santa Maria
Country	Chile
Client	CDEC SIC
Technical Data	4*150 MW / 128 MW / 350 MW / 350 MW – Drum boiler
Scope of Services	Minimum load reduction / ramp rates / start-up optimization – Audit
Project Finalization/ Duration	2015 – 2017

Project	Power Plant Zonguldak Unit 2/3
Country	Turkey
Client	Eren Energji
Technical Data	2*615 MW – Once through boiler
Scope of Services	Minimum load reduction – Study
Project Finalization / Duration	2017 / 3 month

Project	Power Plant Dadri / Simhadri
Country	India
Client	NTPC
Technical Data	210 MW / 500 MW – Drum boiler
Scope of Services	Minimum load reduction / ramp rates / start-up optimization – Study
Project Finalization/ Duration	2017 / 6 month

Project	Power Plant HKW West 2/3
Country	Germany
Client	Mainova
Technical Data	Drum boiler
Scope of Services	1-mill operation – Study as well as test
Project Finalization / Duration	2017

**International
proven
references
by STEAG
Energy Services**

STEAG has unique approach to flexibilization of power plants based on

- **operating expertise**
- **innovative software solutions like PiT-Navigator (APC), Life Time Monitoring System etc.**
- **special engineering services**

This approach has been successfully applied to several power plants !

Time for Flexibilization
by
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